

Grid distortion errors in streamfunction coordinates

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Abstract

Grid distortion errors arising due to the use of non-orthogonal grid in the curvilinear streamfunction coordinate system are analyzed in this work. The objective is to offer a method of measuring and quantifying grid distortion errors. This is accomplished by solving numerically the problem of viscous fluid flow in a curvilinear, two-dimensional channel, governed the the Navier-Stokes equations. The curvilinear flow domain is transformed into a rectangular computational domain, and the governing equations and boundary conditions are transformed, using the von Mises transformation. Grid distortions errors are then quantified using the metrics of transformation, and are taken to be proportional to the angle of inclination to the horizontal of the tangents to the streamlines of the flow. At each grid cell the sine of the inclination angle, defined in terms of the metrics, is computed and the largest possible value is obtained. Effects of the various boundary vorticity approximations on grid distortion are studied in this work where in the process the streamline pattern in the flow

field and the equivorticity curves are obtained for small Re when uniform and non-uniform grids are used.

Keywords: *Grid distortion errors; von Mises; curvilinear coordinates.*

1 Introduction

When finite differences are used to solve partial differential equations with boundary conditions in general coordinate systems (such as fluid flow equations in curvilinear domains), the following are some of the errors and their sources that are introduced in the process and affect the local and global accuracies of the numerical solution obtained (*cf.* [1-5] and the references therein):

- a) Round-off errors due to numerical computations
- b) Solution errors due to the differencing schemes
- c) Errors in the approximation of boundary conditions
- d) Local grid distortion errors due to loss of orthogonality of grid when curvilinear coordinates are used
- e) Errors due to high grid aspect ratios
- f) Additional truncation errors that arise due to the introduction of extra convective terms when using curvilinear coordinates.

In addition to the above, grid size used, grid clustering near the boundary, the order of accuracy of the differencing schemes used in the computational domain and on the boundary, and the choice of uniform or non-uniform (clustered) grid, influence both the local and global accuracy of the numerical solution.

The above factors have been the subject matter of a large number of investigations (*cf.* [6-15] and the references therein), due to the importance of these studies in the efficient design of software and codes with applications to fluid flow and groundwater simulation, [14].

Errors associated with grid distortion are due to the use of non-orthogonal grid and the mapping of a curvilinear region onto a rectangular region. These errors can be measured in terms of angles of deviation from orthogonality of a computational grid. Their influence on local and global accuracies of computed solutions can be quantified in terms of the metrics of the employed transformation by defining the deviation angle in terms of the metrics. Grid distortion errors are therefore dependent in part on: (i) the transformation used, (ii) the shape of the curvilinear boundary, and (iii) the type of grid employed (that is, whether clustered or uniform).

In using uniform grid, it is sometimes possible to arrive at the wrong conclusion that uniform grid produce small grid distortion. If, when using uniform grid, the step size near the boundary is fairly large (non-refined grid) then the effect of the boundary shape is not properly transmitted into the whole computational domain.

This results in a superficial reduction in grid distortion error. For clustered grid with small step size near the boundary, a more accurate effect of the boundary is transmitted into the computational domain and the effect of grid distortion is more pronounced.

In the current work we study grid distortion and the main factors that have an influence on it when the curvilinear domain is mapped onto a rectangular domain using von Mises coordinates, by devising a numerical experiment in which we consider viscous fluid flow through a two-dimensional curvilinear channel. We determine in the computational domain the largest grid distortion errors incurred when different boundary shapes are used and different finite difference approximations are implemented in computing vorticity at the boundaries. Comparison is provided between grid distortion errors when a uniform grid is used and when a grid with a variable step size is used. Grid size used is taken the same for all cases studied and first, second and third-order accurate boundary vorticity schemes are used for the sake of comparison. However, we also study the effect of grid refinement on grid distortion.

To measure the effectiveness of a particular boundary we consider the region near the entrance to the channel. It is expected that the parabolic inlet profile is undisturbed in the first few steps into the channel. This implies that the vorticity along each streamline is constant, and the equivorticity lines should be as close to the horizontal as possible. However, due to boundary vorticity approximations and the influence of boundary shape, the flow pattern is disturbed and the equivorticity lines deviate from the horizontal. In order to place a quantitative measure on the influence of the boundary vorticity approximations, we measure the grid distortion in terms of sine of the angle between the horizontal axis and the tangent to the streamlines of the flow. In the process we solve the governing Navier-Stokes equations, generate streamline patterns and equivorticity curves.

2 Metrics of transformation

Consider the curvilinear net (x, ψ) in which the curves $\psi = \text{constant}$, represent streamlines of the flow. Now, consider the following transformation which defines the von Mises coordinates [16-18]:

$$\left. \begin{array}{l} x = x \\ y = y(x, \psi) \end{array} \right\}. \quad (1)$$

The Jacobian of transformation (1) is defined as

$$J = \frac{\partial(x, y)}{\partial(x, \psi)} = y_\psi, \quad (2)$$

where subscript notation denotes partial differentiation.

Let dS be an element of arc length along any curve in the xy -plane, with the squared element of arc length given by:

$$dS^2 = dx^2 + dy^2. \quad (3)$$

From (1) we obtain:

$$\left. \begin{aligned} dx &= dx \\ dy &= y_x dx + y_\psi d\psi \end{aligned} \right\}. \quad (4)$$

Using (4) in (3), we obtain:

$$dS^2 = E(x, \psi)dx^2 + 2F(x, \psi)dxd\psi + G(x, \psi)d\psi^2, \quad (5)$$

where E, F , and G are the metrics of transformation (coefficients of the first fundamental form) that satisfy:

$$E(x, \psi) = 1 + (y_x)^2, \quad (6)$$

$$F(x, \psi) = y_x y_\psi, \quad (7)$$

$$G(x, \psi) = (y_\psi)^2. \quad (8)$$

Distances in the x - and ψ - directions are given, respectively, by:

$$dS_x = \sqrt{E}dx, \quad (9)$$

$$dS_\psi = \sqrt{E}d\psi, \quad (10)$$

and the Jacobian of transformation (2) is expressed in terms of the metrics as

$$J = \mp \sqrt{EG - F^2}. \quad (11)$$

If fluid flows along the streamline $\psi = c$ in the direction of increasing x , then $J > 0$ and the positive sign in (11) is chosen, while if fluid flows in the direction of decreasing x , then $J < 0$ and the negative sign in (11) is chosen. Now, the

vector $(1, y_x)$ denotes the tangent vector to the curve $\psi = c$, and $(0, y_\psi)$ denotes the tangent vector to the curve $x = \text{constant}$.

Letting $\alpha(x, \psi)$ denote the angle of inclination to the x -axis of the tangent line to $\psi = c$, directed in the sense of increasing x , as shown in Fig. 1, then:

$$\cos \alpha = \frac{1}{|(1, y_x)|} = \frac{1}{\sqrt{1 + (y_x)^2}} = \frac{1}{\sqrt{E}}. \quad (12)$$

$$\sin \alpha = \frac{y_x}{|(1, y_x)|} = \frac{y_x}{\sqrt{1 + (y_x)^2}} = \frac{y_x}{\sqrt{E}}. \quad (13)$$

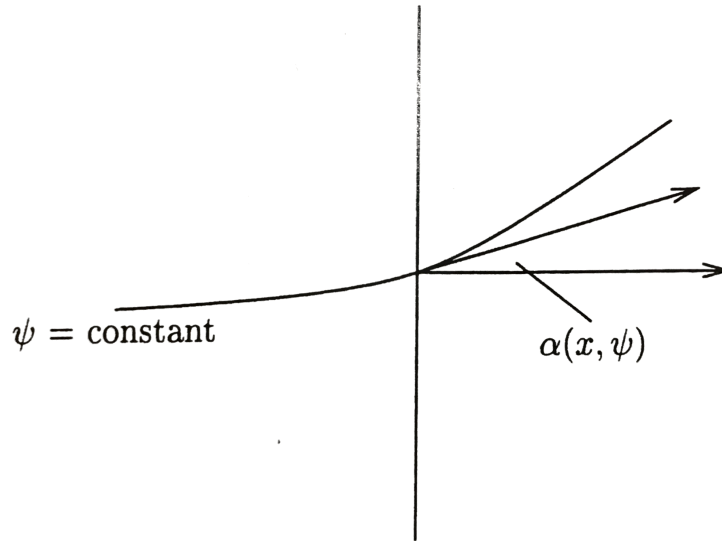


Fig. 1. Representative sketch: Angle of inclination.

Equations (12) and (13) provide a measure of the physical orientation of the computational grid relative to the x -axis. Along the x -axis, $y_x = 0$ or $\cos \alpha = 1$, hence $\alpha = 0$. Grid aspect ratio, AR , is the ratio of the magnitudes of the tangent vectors, expressed as

$$AR = \frac{\Delta S_\psi}{\Delta S_x} = \frac{\sqrt{(y_\psi)^2}}{\sqrt{1 + (y_x)^2}} \frac{\Delta \psi}{\Delta x} = \sqrt{\frac{G}{E}} \frac{\Delta \psi}{\Delta x} \quad (14)$$

There are two parts of grid aspect ratio (14), the first is the **controllable ratio of grid spacing** $\frac{\Delta \psi}{\Delta x}$ which depends on one's choice of grid size or grid spacings.

The second is the **uncontrollable ratio** $\frac{\sqrt{(y_\psi)^2}}{\sqrt{1+(y_x)^2}}$, which is inherent in the curvilinear coordinate system used. The **local grid distortion** is determined by angle $\mathcal{G} = \frac{\pi}{2} - \alpha$ between the coordinate lines, measured by:

$$\cos \mathcal{G} = \sin \alpha = \frac{y_x}{\sqrt{1+(y_x)^2}} = \frac{F}{\sqrt{EG}}. \quad (15)$$

Accuracy of the solution is degraded by this grid distortion. Therefore, for high accuracy, the grid should be orthogonal or near orthogonal. For orthogonal grid, $\mathcal{G} = \frac{\pi}{2}$ or $\cos \mathcal{G} = \sin \alpha = 0$. Equivalently, $F = y_x y_\psi = 0$, which implies that $y_x = 0$ or $y_\psi = 0$. If $y_\psi = 0$ then $AR = 0$ (which is impossible), while if $y_x = 0$ then $AR = y_\psi$. If the grid is not orthogonal, additional truncation errors are introduced and are proportional to $\cos \mathcal{G}$. However, it is generally accepted that departure from orthogonality of up to $\frac{\pi}{4}$ radians can be tolerated, [1].

3 Numerical experiment

3.1 Physical domain quantities and equations

In order to study the effect of grid distortion, error propagation, accuracy of the numerical solution and convergence of the numerical scheme used, we consider the flow of a viscous fluid through a two-dimensional channel shown diagrammatically in Fig. 2, and described by:

$$\{(x, y) | x_{\min} \leq x \leq x_{\max}; f_1(x) \leq y \leq f_2(x)\} \quad (16)$$

Fluid enters through section ad and exits through bc . The channel is assumed to be long enough to impose parallel flow at its inlet and exit.

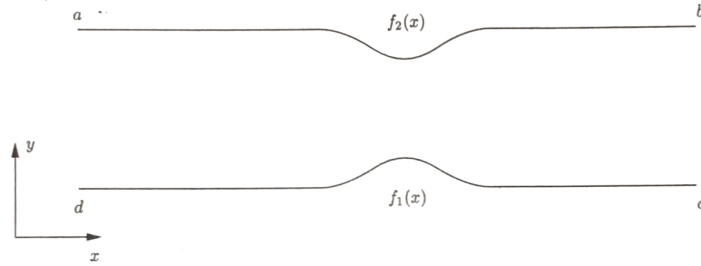


Fig. 2. Physical domain: two-dimensional channel

Equations governing the flow are the two-dimensional Navier-Stokes equations in the following dimensionless vorticity-streamfunction, $\omega-\psi$ form:

Streamfunction equation:

$$\psi_{xx} + \psi_{yy} = -\omega. \quad (17)$$

Vorticity equation:

$$\omega_{xx} + \omega_{yy} = \text{Re}[\psi_y \omega_x - \psi_x \omega_y]. \quad (18)$$

Relationships between the velocity components, u, v , the streamfunction, ψ , and vorticity, ω , are given by:

$$u = \psi_y, \quad (19)$$

$$v = -\psi_x, \quad (20)$$

$$\omega = v_x - u_y. \quad (21)$$

Physical boundary conditions are the no-slip on the channel walls and a parallel, parabolic velocity profile at the inlet and exit of the channel, namely:

For $x_{\min} \leq x \leq x_{\max}$

$$u(x, f_1(x)) = u(x, f_2(x)) = 0, \quad (22)$$

$$v(x, f_1(x)) = v(x, f_2(x)) = 0. \quad (23)$$

For $f_1(x) \leq y \leq f_2(x)$

$$u(x_{\min}, y) = u(x_{\max}, y) = 1 - y^2, \quad (24)$$

$$v = v_x = 0 \text{ at } (x_{\min}, y) \text{ and } (x_{\max}, y). \quad (25)$$

Corresponding conditions on the streamfunction and vorticity are the following inlet and exit conditions:

For $f_1(x) \leq y \leq f_2(x)$

$$\psi(x_{\min}, y) = \psi(x_{\max}, y) = y - \frac{y^3}{3}, \quad (26)$$

$$\omega(x_{\min}, y) = \omega(x_{\max}, y) = 2y. \quad (27)$$

For $x_{\min} \leq x \leq x_{\max}$

$$\psi(x, f_1(x)) = \psi_{\min}, \quad (28)$$

$$\psi(x, f_2(x)) = \psi_{\max}, \quad (29)$$

$$\omega(x, f_1(x)) = (v_x - u_y) \Big|_{y=f_1(x)}, \quad (30)$$

$$\omega(x, f_2(x)) = (v_x - u_y) \Big|_{y=f_2(x)}. \quad (31)$$

3.2 Computational domain quantities and equations

In order to solve the governing equations using finite differences, the curvilinear physical domain is mapped onto a rectangular computational domain, Fig. 3, using the von Mises transformation (1). Boundary conditions and governing equations are transformed into von Mises coordinates, as described in what follows. Using transformation (1), the roles of ψ and y are interchanged, the curvilinear streamlines, $\psi = \text{constant}$, in the physical domain are horizontal straight lines in the computational domain, and the physical domain is mapped onto the rectangular computational domain described by:

$$\{(x, \psi) \mid x_{\min} \leq x \leq x_{\max}; \psi_{\min} \leq \psi \leq \psi_{\max}\} \quad (32)$$

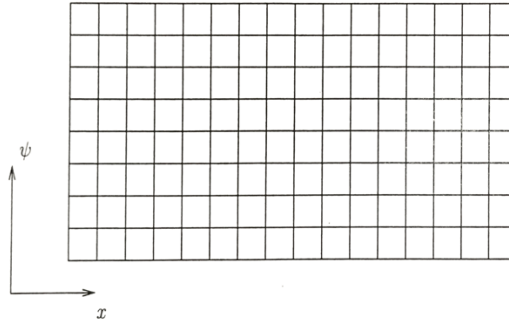


Fig. 3. Rectangular Computational domain.

It is clear that the lower and upper boundaries are the streamlines ψ_{\min} and ψ_{\max} , respectively.

First-order partial differential operators in the Cartesian and von Mises coordinate systems are related by:

$$\partial_x = \partial_x - \frac{y_x}{y_\psi} \partial_\psi, \quad (33)$$

$$\partial_y = \frac{1}{y_\psi} \partial_\psi, \quad (34)$$

and higher-order operators can be obtained by repeated applications of (33) and (34) onto themselves. Governing equations (17) and (18) are thus transformed into the following forms, to be solved for $y(x, \psi)$ and $\omega(x, \psi)$:

The y – equation:

$$L[y] = \omega(y_\psi)^3. \quad (35)$$

The ω – equation:

$$L[\omega] = (y_\psi)^2 \omega \omega_\psi + \text{Re } y_\psi \omega_x, \quad (36)$$

where

$$L \equiv (y_\psi)^2 \partial_{xx} - 2y_x y_\psi \partial_{x\psi} + [1 + (y_x)^2] \partial_{\psi\psi}. \quad (37)$$

Velocity components take the following forms in von Mises coordinates

$$u = \frac{1}{y_\psi}, \quad (38)$$

$$v = \frac{y_x}{y_\psi} = uy_x. \quad (39)$$

and the square of the speed of the flow is given by:

$$q^2 = u^2 + v^2 = \frac{1 + (y_x)^2}{(y_\psi)^2}. \quad (40)$$

Equations (35) and (36) are to be solved in the computational domain subject to the following transformed conditions on $y(x, \psi)$ and $\omega(x, \psi)$:

For $x_{\min} \leq x \leq x_{\max}$

$$y(x, \psi_{\min}) = f_1(x), \quad (41)$$

$$y(x, \psi_{\max}) = f_2(x), \quad (42)$$

$$\omega(x, \psi_{\min}) = v_x - \frac{1}{2}(q^2)_\psi \Big|_{(x, \psi_{\min})}, \quad (43)$$

$$\omega(x, \psi_{\max}) = v_x - \frac{1}{2}(q^2)_\psi \Big|_{(x, \psi_{\max})}. \quad (44)$$

For $\psi_{\min} \leq \psi \leq \psi_{\max}$

$$y(x_{\min}, \psi) - \frac{y^3(x_{\min}, \psi)}{3} = \psi, \quad (45)$$

$$y(x_{\max}, \psi) - \frac{y^3(x_{\max}, \psi)}{3} = \psi, \quad (46)$$

$$\omega(x_{\min}, \psi) = 2y(x_{\min}, \psi), \quad (47)$$

$$\omega(x_{\max}, \psi) = 2y(x_{\max}, \psi). \quad (48)$$

4 Finite difference approximations

4.1 Discretizing the flow domain

In order to solve (35) and (36) numerically, subject the transformed boundary conditions (41)-(48), the computational domain is discretized using either a uniform grid or a non-uniform grid, with vertical grid lines ranging from $i=1$ at

x_{\min} to $i=Imax$ at x_{\max} , and horizontal grid lines ranging from $j=1$ at ψ_{\min} to $j=Jmax$ at ψ_{\max} .

In this work, we choose the following data for the computational domain:

$$f_1(x) = \begin{cases} -1; |x| > 1 \\ -1 + k(1 + \cos \pi x); |x| \leq 1 \end{cases}; x_{\min} \leq x \leq x_{\max} \quad (49)$$

$$f_2(x) = \begin{cases} 1; |x| > 1 \\ 1 - k(1 + \cos \pi x); |x| \leq 1 \end{cases}; x_{\min} \leq x \leq x_{\max} \quad (50)$$

where k is a *shape parameter* that controls the thickness of the boundary bump, and $x_{\min} = -4; x_{\max} = 4; \psi_{\min} = -\frac{2}{3}; \psi_{\max} = \frac{2}{3}$.

The horizontal extent of the channel is deemed to be sufficient to impose parallel inlet and exit velocity profiles. We select $Imax = 201$ grid points in the x -direction and $Jmax = 51$ grid points in the ψ -direction.

In using uniform grid, step sizes are constant and take the values $\Delta x = 0.04$ and $\Delta \psi \approx 0.0267$. The choice of constant step size in the ψ -direction in the computational domain produces a grid in the physical domain that is clustered near the horizontal centerline of the channel, away from the boundary, [3,4]. This is a disadvantage of using uniform grid, since one desires clustering near the boundary in order to better capture boundary effects.

In using non-uniform grid, a convenient way of generating clustered grid near the computational boundary is to select in the physical domain constant steps in the y -direction and to use (26) to compute the ψ -values in the computational domain, hence determine the step sizes in the ψ -direction. This method produces a naturally clustered grid near the computational boundary that is tied to the inlet velocity profile [3]. This is one of the advantages of using the von Mises transformation.

Now, at the inlet to the channel, $-1 \leq y \leq 1$, and using 51 grid points in the y -direction gives $\Delta y = 0.04$ in the physical domain. We can then generate the set of y -values $\{y_j; j = 1, 2, \dots, 51\} = \{-1, -0.96, -0.92, \dots, 1\}$ and calculate the corresponding ψ_j using (26). We generate values for the variable step sizes $\Delta \psi_j$ using the three grid points $(i, j-1), (i, j), (i, j+1)$, by defining for $j = 2$ to $Jmax-1$:

$$\Delta\psi_j = \psi_{j+1} - \psi_j, \quad (51)$$

$$\Delta\psi_{j-1} = \psi_j - \psi_{j-1}. \quad (52)$$

4.2 Discretizing the governing equations

Expansion of a function $F(x, \psi)$ about the point (i, j) and using Taylor series approximations, we obtain the following second-order finite difference expressions for the first and second derivatives with respect to x and ψ , valid for variable step size in the ψ -direction:

$$\left. \frac{\partial F}{\partial x} \right|_{i,j} \approx \frac{F_{i+1,j} - F_{i-1,j}}{2\Delta x}, \quad (53)$$

$$\left. \frac{\partial F}{\partial \psi} \right|_{i,j} \approx \frac{F_{i,j+1} - F_{i,j-1}}{\Delta\psi_j + \Delta\psi_{j-1}}, \quad (54)$$

$$\left. \frac{\partial^2 F}{\partial x^2} \right|_{i,j} \approx \frac{F_{i+1,j} - 2F_{i,j} + F_{i-1,j}}{\Delta x^2}, \quad (55)$$

$$\left. \frac{\partial^2 F}{\partial \psi^2} \right|_{i,j} \approx 2 \left(\frac{F_{i,j+1} - (1 + \beta_j)F_{i,j} + \beta_j F_{i,j-1}}{\Delta\psi_j^2 + \Delta\psi_j \Delta\psi_{j-1}} \right), \quad (56)$$

$$\left. \frac{\partial^2 F}{\partial x \partial \psi} \right|_{i,j} \approx \frac{F_{i+1,j+1} + F_{i-1,j-1} - F_{i+1,j-1} - F_{i-1,j+1}}{2\Delta x \Delta\psi_j + 2\Delta x \Delta\psi_{j-1}}, \quad (57)$$

where F stands for either of the unknowns ω or y , and

$$\beta_j = \frac{\Delta\psi_j}{\Delta\psi_{j-1}}. \quad (58)$$

Applying approximations (53)-(58) to the y - and ω -equations (35) and (36), we obtain discretized forms of the equations which are then written in the following tri-diagonal matrix form that is suitable for *Successive Line Over Relaxation* (SLOR) in the j -direction with sweep in the i -direction:

$$a_{i,j} F_{i,j-1} + b_{i,j} F_{i,j} + c_{i,j} F_{i,j+1} = B_{i,j}, \quad (59)$$

where $F_{i,j}$ stands for $y_{i,j}$ or $\omega_{i,j}$, and $B_{i,j}$ is the right-hand-side vector. The matrix coefficients $a_{i,j}, b_{i,j}, c_{i,j}$, and the right-hand-side vector $B_{i,j}$ are given for each of governing equations (35) and (36) in what follows, for $i=2,3,\dots,Imax-1$, and $j=2,3,\dots,Jmax-1$.

For the y-equation:

$$a_{i,j} = (1 + \beta_j) \{4\Delta x^2 + (y_{i+1,j} - y_{i-1,j})^2\} \quad (60)$$

$$b_{i,j} = -4(y_{i,j+1} - y_{i,j-1})^2 - \frac{(1 + \beta_j)^2}{\beta_j} \{4\Delta x^2 + (y_{i+1,j} - y_{i-1,j})^2\} \quad (61)$$

$$c_{i,j} = \left(\frac{1 + \beta_j}{\beta_j}\right) \{4\Delta x^2 + (y_{i+1,j} - y_{i-1,j})^2\} \quad (62)$$

$$B_{i,j} = -2(y_{i,j+1} - y_{i,j-1})^2 (y_{i+1,j} + y_{i-1,j}) + 2 \left(\frac{\Delta x^2}{\Delta \psi_j + \Delta \psi_{j-1}}\right) (y_{i,j+1} - y_{i,j-1})^3 \omega_{i,j} \quad (63)$$

$$+ (y_{i+1,j} - y_{i-1,j})(y_{i,j+1} - y_{i,j-1}) \{y_{i+1,j+1} + y_{i-1,j-1} - y_{i+1,j-1} - y_{i-1,j+1}\}$$

For the ω -equation:

$$a_{i,j} = 2\beta_j (\Delta \psi_j + \Delta \psi_{j-1}) \left[1 + \left(\frac{y_{i+1,j} - y_{i-1,j}}{2}\right)^2\right] \quad (64)$$

$$b_{i,j} = -2(y_{i,j+1} - y_{i,j-1})^2 - 2(1 + \beta_j) (\Delta \psi_j + \Delta \psi_{j-1}) \left[1 + \left(\frac{y_{i+1,j} - y_{i-1,j}}{2}\right)^2\right] \quad (65)$$

$$c_{i,j} = 2(\Delta \psi_j + \Delta \psi_{j-1}) \left[1 + \left(\frac{y_{i+1,j} - y_{i-1,j}}{2}\right)^2\right] \quad (66)$$

$$B_{i,j} = (y_{i,j+1} - y_{i,j-1})^2 \left\{ \frac{\Delta x^2}{\Delta \psi_j + \Delta \psi_{j-1}} \omega_{i,j} (\omega_{i,j+1} - \omega_{i,j-1}) - (\omega_{i+1,j} + \omega_{i-1,j}) \right\}$$

$$+ \frac{\Delta x \text{ Re}}{2} (\Delta \psi_j + \Delta \psi_{j-1}) (y_{i,j+1} - y_{i,j-1}) (\omega_{i+1,j} - \omega_{i-1,j}) \quad (67)$$

$$+ (y_{i+1,j} - y_{i-1,j})(y_{i,j+1} - y_{i,j-1}) \left\{ \frac{\omega_{i+1,j+1} + \omega_{i-1,j-1} - \omega_{i+1,j-1} - \omega_{i-1,j+1}}{2} \right\}$$

4.3 Boundary vorticity approximations

Vorticity on the lower and upper boundaries is given by (43) and (44), respectively, in terms of the first derivative of the square of the speed of the flow. Boundary vorticity is approximated using the following finite difference expressions of first, second and third order accuracy for the first derivative of the square of the speed, for both uniform and non-uniform grid. For first-order accurate approximation we implement 2, 3, 4, and 5 grid points using schemes derived in [4]. Reference to these schemes is as follows: a (1,2) scheme uses the grid points along $j=1$ and $j=2$, while a (1,2,3,4,5) scheme uses grid points along $j=1,2,3,4,5$.

For non-uniform grid, first, second and third-order accurate forward schemes, respectively, using the natural order of grid lines, are:

First-order Schemes:

(1,2) Scheme

$$\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx -\frac{1}{2} \frac{(q^2)_{i,2} - (q^2)_{i,1}}{\Delta\psi_1} . \quad (68)$$

(1,2,3) Scheme

$$\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx -\frac{1}{2} \frac{(q^2)_{i,3} + (q^2)_{i,2} - 2(q^2)_{i,1}}{2\Delta\psi_1 + \Delta\psi_2} \quad (69)$$

(1,2,3,4) Scheme

$$\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx -\frac{1}{2} \frac{(q^2)_{i,4} + (q^2)_{i,3} + (q^2)_{i,2} - 3(q^2)_{i,1}}{3\Delta\psi_1 + 2\Delta\psi_2 + \Delta\psi_3} \quad (70)$$

(1,2,3,4,5) Scheme

$$\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx -\frac{1}{2} \frac{(q^2)_{i,5} + (q^2)_{i,4} + (q^2)_{i,3} + (q^2)_{i,2} - 4(q^2)_{i,1}}{4\Delta\psi_1 + 3\Delta\psi_2 + 2\Delta\psi_3 + \Delta\psi_4} \quad (71)$$

Second-order (1,2,3) Scheme

$$\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx -\frac{1}{2} \left[-\frac{(2\Delta\psi_1 + \Delta\psi_2)}{\Delta\psi_1(\Delta\psi_1 + \Delta\psi_2)} q_{i,1}^2 + \frac{(\Delta\psi_1 + \Delta\psi_2)}{\Delta\psi_1\Delta\psi_2} q_{i,2}^2 - \frac{\Delta\psi_1}{(\Delta\psi_1 + \Delta\psi_2)\Delta\psi_2} q_{i,3}^2 \right] \quad (72)$$

Third-order (1,2,3,4) Scheme

$$\begin{aligned}
\omega_{i,1} = -\frac{1}{2}(q^2_\psi)_{i,1} \approx & -\frac{1}{2} \left[-\left\{ \frac{\Delta\psi_1(\Delta\psi_1 + \Delta\psi_2) + (\Delta\psi_1 + \Delta\psi_2 + \Delta\psi_3)(2\Delta\psi_1 + \Delta\psi_2)}{\Delta\psi_1(\Delta\psi_1 + \Delta\psi_2)(\Delta\psi_1 + \Delta\psi_2 + \Delta\psi_3)} \right\} (q^2)_{i,1} \right. \\
& + \left\{ \frac{(\Delta\psi_1 + \Delta\psi_2) + (\Delta\psi_1 + \Delta\psi_2 + \Delta\psi_3)}{\Delta\psi_1\Delta\psi_2(\Delta\psi_2 + \Delta\psi_3)} \right\} (q^2)_{i,2} \\
& - \left\{ \frac{\Delta\psi_1(\Delta\psi_1 + \Delta\psi_2 + \Delta\psi_3)}{\Delta\psi_2\Delta\psi_3(\Delta\psi_1 + \Delta\psi_2)} \right\} (q^2)_{i,3} \\
& \left. + \left\{ \frac{\Delta\psi_1(\Delta\psi_1 + \Delta\psi_2)}{\Delta\psi_3(\Delta\psi_2 + \Delta\psi_3)(\Delta\psi_1 + \Delta\psi_2 + \Delta\psi_3)} \right\} (q^2)_{i,4} \right] \quad (73)
\end{aligned}$$

Expressions (68)-(73) are forward schemes applied at the lower boundary using grid points $(i,1), (i,2), (i,3), (i,4)$ and $(i,5)$. Similar, backward schemes are used on the upper boundary using grid points $(i, J_{\max}), (i, J_{\max-1}), (i, J_{\max-2}), (i, J_{\max-3})$ and $(i, J_{\max-4})$.

For uniform grid, first, second and third-order accurate forward schemes, respectively, are:

$$(q^2_\psi)_{i,1} \approx \frac{(q^2)_{i,2} - (q^2)_{i,1}}{h} \quad (74)$$

$$(q^2_\psi)_{i,1} \approx \frac{-3q^2_{i,1} + 4q^2_{i,2} - q^2_{i,3}}{2h} \quad (75)$$

$$(q^2_\psi)_{i,1} \approx \frac{2(q^2)_{i,4} - 9(q^2)_{i,3} + 18(q^2)_{i,2} - 11(q^2)_{i,1}}{6h}. \quad (76)$$

Similar, backward-differences schemes can be developed for boundary vorticity at the upper boundary.

4.4 Velocity components' approximations

Velocity components, given by (38) and (39), are discretized using (53) and (54) to obtain, for $i = 2, 3, \dots, i = 1, 2, \dots, J_{\max-1}$ and $j = 1, 2, \dots, J_{\max-1}$:

$$u_{i,j} = \frac{\Delta\psi_j + \Delta\psi_{j-1}}{y_{i,j+1} - y_{i,j-1}} \quad (77)$$

$$v_{i,j} = u_{i,j} \frac{y_{i+1,j} - y_{i-1,j}}{2\Delta x} \quad (78)$$

or

$$v_{i,j} = \left(\frac{\Delta\psi_j + \Delta\psi_{j-1}}{2\Delta x} \right) \frac{y_{i+1,j} - y_{i-1,j}}{y_{i,j+1} - y_{i,j-1}}. \quad (79)$$

For uniform grid, equations (77) and (79) take the forms, respectively:

$$u_{i,j} = \frac{2\Delta\psi}{y_{i,j+1} - y_{i,j-1}} \quad (80)$$

$$v_{i,j} = \frac{\Delta\psi}{\Delta x} \frac{y_{i+1,j} - y_{i-1,j}}{y_{i,j+1} - y_{i,j-1}}. \quad (81)$$

4.5 Solution algorithm

Numerical solution to the governing equations, subject to the given boundary conditions, is obtained according to the following algorithm:

Step 1:

- (a) Assign values to I_{\max} , J_{\max} , x_{\min} , x_{\max} , $y_{\min} = f_1(x_{\min})$, $y_{\max} = f_2(x_{\min})$, ψ_{\min} , ψ_{\max} .
- (b) Compute $\Delta x = \frac{x_{\max} - x_{\min}}{I_{\max} - 1}$ and $\Delta y = \frac{y_{\max} - y_{\min}}{J_{\max} - 1}$.
- (c) Compute $x_i \equiv x(i,1) = x(i, J_{\max}) = x_{\min} + (i-1)\Delta x$ for $i = 2, 3, \dots, I_{\max} - 1$ and $y_j \equiv y(1, j) = y(I_{\max}, j) = y_{\min} + (j-1)\Delta y$ for $j = 2, 3, \dots, J_{\max} - 1$.
- (d) Compute $f_1(x_i)$ and $f_2(x_i)$ for $i = 1, 2, \dots, I_{\max}$ using equations (49) and (50).
- (e) Compute $\psi_j = y_j - \frac{y_j^3}{3}$ and $\Delta\psi_j = \psi_{j+1} - \psi_j$ for $j = 1, 2, \dots, J_{\max} - 1$.
- (f) Assign, and compute, values of the boundary and entry conditions as follows:
For $i = 2, 3, \dots, I_{\max} - 1$:
 $\psi(i,1) = \psi_{\min}$

$$\begin{aligned}
\psi(i, J_{\max}) &= \psi_{\max} \\
u(i, 1) &= 0 \\
u(i, J_{\max}) &= 0 \\
v(i, 1) &= 0 \\
v(i, J_{\max}) &= 0
\end{aligned}$$

For $j = 1, 2, \dots, J_{\max}$

$$\begin{aligned}
v(1, j) &= 0 \\
v(I_{\max}, j) &= 0 \\
u(1, j) &= 1 - (y_j)^2 \\
u(I_{\max}, j) &= 1 - (y_j)^2 \\
\omega(1, j) &= 2y_j \\
\omega(I_{\max}, j) &= 2y_j
\end{aligned}$$

- (g) Initialize $\omega_{i,j}$ and $y_{i,j}$ at interior grid points by assigning them small starting values, for $i = 2, 3, \dots, I_{\max-1}$ and $j = 2, 3, \dots, J_{\max-1}$.

Step 2:

- Calculate $u_{i,j}$ and $v_{i,j}$ at interior grid points using expressions (77)-(81).
- Calculate the boundary vorticity using expressions (68)-(76).

Step 3:

- Calculate coefficients of the tri-diagonal systems appearing in (60)-(67).
- Solve the ω - and y -equations using the tri-diagonal solver and successive line over-relaxation according to:

$$F_{i,j}^{n+1} = F_{i,j}^n + r[F_{i,j}^{*n+1} - F_{i,j}^n] \quad (82)$$

where r is the relaxation parameter, $F_{i,j}^{*n+1}$ is the value of $y_{i,j}$ or $\omega_{i,j}$ at iteration level $n+1$, obtained from the tri-diagonal solver, $F_{i,j}^n$ is the value at iteration level n , and $F_{i,j}^{n+1}$ is the most up-to-date value.

Step 4: Repeat steps 2 and 3 until the following convergence criterion is satisfied:

$$|F_{i,j}^{n+1} - F_{i,j}^n| \leq 5 \times 10^{-6}. \quad (83)$$

Step 5: After convergence, repeat step 2.

5 Results and discussion

5.1 Grid Distortion

Grid distortion measurements have been obtained for grid size of 201×51 . Results have been obtained for variable step schemes of first, second and third order accuracy and comparison is made with uniform grid results. The values of $\cos \mathcal{G}$ are calculated using equation (15) in discretized form. Locations of maximum distortion are not reported here as they occur, within error tolerance of 5×10^{-6} , at a fairly large number of points in the flow field.

Table 1: Distortion data. $k = 1/24$, $\Delta x = 0.04$.

*: Using uniform grid. **: $k = 1/20$. ***: $\Delta x = 0.02$; $k = 1/24$

Scheme	Order	Maximum Distortion	Number of Iterations
(1,2)	1	0.117612	194
(1,2)*	1		236
(1,2,3)	1	0.130447	196
(1,2,3,4)	1	0.148066	203
(1,2,3,4,5)	1	0.159754	213
(1,2,3)	2	0.117634	204
(1,2,3)*	2		233
(1,2,3)**	2	0.156425	260
(1,2,3,4)	3	0.117504	204
(1,2,3,4)**	3	0.155991	426
(1,2,3,4)***	3	0.117883	451

Table 1 illustrates the distortion measurements for first-order accurate boundary vorticity schemes that use 2, 3, 4 and 5 grid points, together with 3-point second-order accurate and 4-point third-order accurate schemes. For first-order schemes with variable step size, increasing the number of grid points used in boundary vorticity schemes results in an increase in the maximum distortion values. This means that the distortion angle \mathcal{G} decreases, and α increases. When second- and third-order schemes are used, values of maximum distortion are comparable with those obtained when using the two-point (1,2) scheme of first-order accuracy. Number of iterations required for convergence are reported in Table 1, which shows an increase in the required number of iterations with increasing scheme accuracy and with increasing number of grid points used in the boundary vorticity approximations.

5.2 Effect of boundary shape

Equations (16) and (17) define the shape of the lower and upper channel boundaries. Thickness of the bump on the boundaries is controlled by parameter k . We have experimented with the following values: $k = \frac{1}{12}, \frac{1}{18}, \frac{1}{20}, \frac{1}{24}$ and found

that when selecting $k > \frac{1}{20}$ with non-uniform grid, an overflow error occurs. This

may be attributed to the closeness of streamlines to the boundary when the bump is thick, and the tendency of flow to approach separation threshold and the development of recirculating eddies near the leading and trailing edges. This kind of flow reversal changes the sign of the Jacobian of transformation, which is a drawback of using the von Mises transformation for viscous fluid flow. Results in this work are therefore based on $k = \frac{1}{24}$ and $k = \frac{1}{20}$, and Table 1 demonstrates

the increase in maximum grid distortion with increasing bump thickness when second- and third-order accurate boundary vorticity schemes are used.

5.3 Effect of grid refinement

If the number of grid points in the x -direction is doubled so that the grid size is 401×51 and $\Delta x = 0.02$, the third-order accurate boundary vorticity scheme produces a maximum distortion of 0.117883. Using this fine grid produces a slightly more accurate results. When using clustered grid, our numerical experiment showed that using grids containing more than 90 grid lines in the ψ -direction results in no convergence. The upper limit on the grid size depends on the boundary vorticity finite difference formula used. For the third-order accurate scheme, the upper limit is 70 lines, while for the first-order accurate (1,2) scheme the limit is 102 lines. These upper limits represent the threshold for detection of viscous separation near the leading or trailing edges of the boundary bump, which results in flow reversal and a change of sign of the Jacobian, hence convergence is hindered.

5.4 Flow patterns and equivorticity curves

Results in this section are based on grid size of 201×51 with boundary vorticity computed using third-order accurate schemes, for both uniform and non-uniform grids.

Streamlines of the flow for $Re = 0$ are illustrated in Fig. 4(a,b). For uniform grid, Fig. 4(a) demonstrates a loss of accuracy in the solution near the inlet and exit to the channel due to lack of clustering near the boundary. In using uniform grid, equal step sizes in the ψ -direction in the computational domain results in clustering near the centre of the channel and the boundary effects are not

efficiently captured in the solution. In using non-uniform grid, Fig. 4(b), illustrates the streamline pattern with a more accurate, expected behaviour near the inlet and exit of the channel. We note that a non-uniform, clustered grid in the computational domain, with clustering near the boundary and capturing boundary effects more accurately, results in a uniform grid in the physical domain.

Streamline patterns have also been obtained for $Re = 20$ and 40 , and exhibit similar qualitative behaviors to the patterns in Fig. 4(a,b), hence not shown here. However, effects of Re are better captured and illustrated in the equivorticity curves, shown in Fig. 5(a,b) and Fig. 6(a,b). As Re increases, the region between two equivorticity curves closest to the trailing edge gets larger. This is indicative of the possibility of potential viscous separation near the trailing edge, with increasing Re , and the potential formation of a recirculating eddy in that region. This behavior persists when either uniform or non-uniform grid is used. The effect of using non-uniform grid is, again, reflected in capturing the boundary effects better than uniform grid, hence producing different values of equivorticity curves near the boundary (along the same computational gridlines).

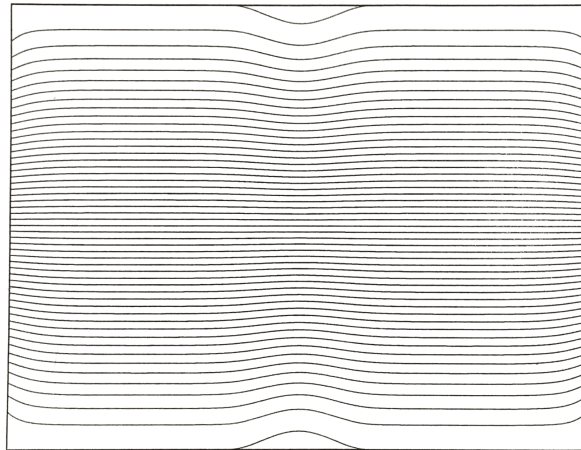


Fig. 4(a). Streamline pattern, uniform grid, $Re = 0$.

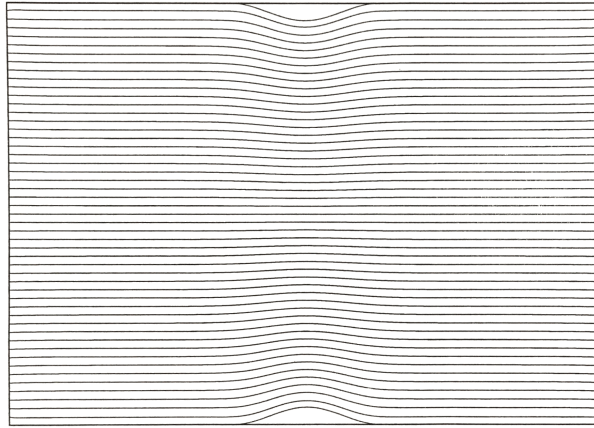


Fig. 4(b). Streamline pattern, clustered grid, $Re = 0$.

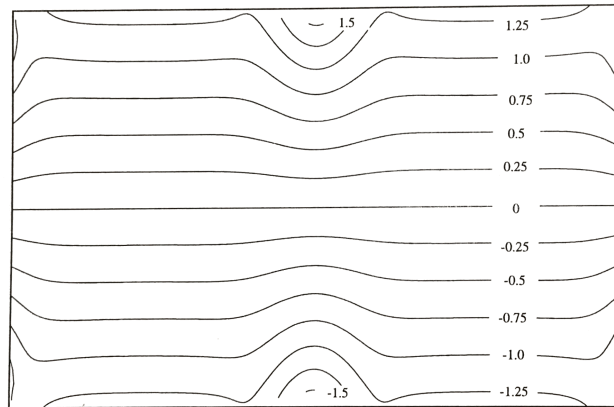


Fig. 5(a). Equivorticity curves, uniform grid, $Re = 0$.

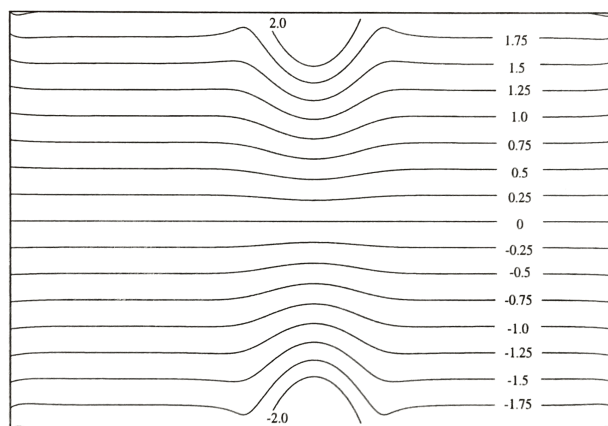


Fig. 5(b). Equivorticity curves, clustered grid, $Re = 0$.

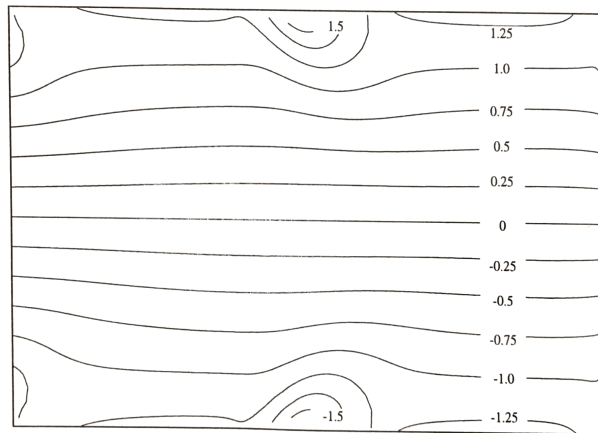


Fig. 6(a). Equivorticity curves, uniform grid, $Re = 40$.

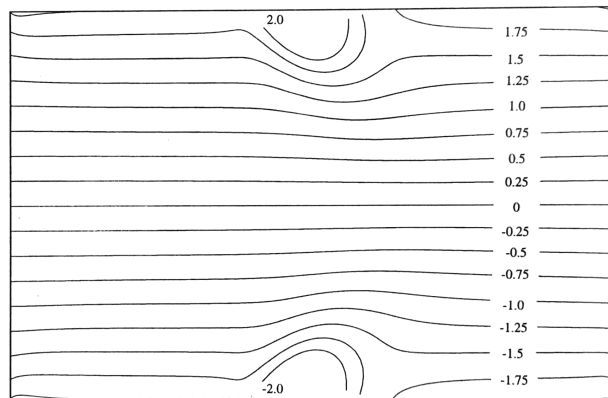


Fig. 6(b). Equivorticity curves, clustered grid, $Re = 40$.

6 Conclusion

In this work we studied grid distortion errors that arise when the von Mises transformation is used in the study of viscous fluid flow through a curvilinear domain. Maximum distortion was quantified using sine of the angle between the tangent to the streamlines and the x -axis. Effects of order of accuracy of the numerical schemes used in computing boundary vorticity and effects of grid refinement on grid distortion have been analyzed. In the process of grid distortion quantification, we produced streamline patterns and equivorticity curves of the flow for small values of Reynolds number.

7 Open problem

In the above analysis we considered grid distortion in a curvilinear domain with boundary bump thickness $k \leq \frac{1}{20}$ so that viscous separation does not occur.

When $k > \frac{1}{20}$ there is a possibility of flow separation near the leading and trailing edges of the bump and a reversal in the value of the Jacobian of transformation. Handling this case requires domain decomposition and the determination of flow separation regions, which is not considered in this work.

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